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EP 0 160 014 B1

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Description**FIELD OF INVENTION**

5 This invention relates to a method of filtration in which cleaning of the filters is affected by a procedure involving back-washing with a pressurised gas. It particularly relates to a method of filtration using filters made of hollow fibres having a pore size in the range from 5 μm to 0.01 μm and to the cleaning of such filters.

BACKGROUND ART

Membrane fouling is generally recognised as the outstanding problem in modern ultrafiltration. A full discussion of the problems can be found in "Fifteen Years of Ultrafiltration" by Michaels, A.S. in Ultrafiltration Membranes and Applications edited by A.R. Cooper (American Chemical Society Symposium, Washington, 9-14 September, 1979, Plenum Press, New York (1980); ISBN 0-306-40548-2) where it stated:

"the problems of reduced throughput, capacity, increased power consumption, compromised separation capability, and reduced membrane service lifetime associated with macro-, solute- and colloid-fouling of ultrafiltration membranes have stubbornly resisted adequate solution despite ten years of engineering experience in pilot- and full-scale industrial situations."

20 According to Michaels, back-washing by reverse flow of permeate in hollow-fibre membrane modules, significantly aids unplugging of membrane pores and detachment of adhering deposits. However, there are only two specific examples of permeate back-washing described in this text and these concern filtration of town water and of electro-deposition paints emulsified in water.

As set forth at pages 109 to 127 of the above text, back-washing of hollow fibres with permeate is used where operating transmembrane pressures are only about one atmosphere so that particles are not driven hard into membrane pores during the filtering process. As indicated above, permeate back-washing has been used where the fouling species are in liquid paint emulsion droplets as these species do not wedge into the membrane pores as do solids. As the transmembrane flux is often only five to twenty litres per square metre per hour ($\text{L/m}^2 \text{ hr}$), the corresponding fluid velocity is only a few millimetres per hour and there is, therefore, no possibility of a high velocity cleaning action.

Permeate back-washing is, in essence, a recycling process and thus a sacrifice of production rate is only justified when the cleaning effect is significant. Some sticky natural wastes (such as brewing residues, starch, and egg) are not removed to any appreciable extent by permeate back-washing. Permeate back-washing is, by definition, a purely hydraulic flow through totally wetted pores of the ultrafiltration membrane. Hollow, porous fibre ultrafilters are preferred where back-wash cleaning is needed because of the structure of the hollow fibres.

Back-washing with compressed air introduced into the hollow filament membranes made of polyvinyl alcohol so as to make them oscillate has been proposed in JP-A-53108882 for cleaning a filter made by binding several tens to several hundreds of thousands of such hollow filament membranes into a bundle. GB-A-1535832 describes back-washing of a semi-permeable membrane with liquid followed by back-washing with gas.

DISCLOSURE OF INVENTION

45 It is an object of this invention to provide an improved method of filtration which involves back-washing hollow fibre filters with gas as the back-wash medium.

According to the present invention there is provided a method of filtering a liquid suspension feedstock in a filter in which the feedstock to be filtered is applied to the outside of a plurality of porous hollow fibres having pores in the range from 5 μm (5 micron) to 0.01 μm (0.01 micron) and the filtrate or permeate is drawn off from the fibre lumens and in which the fibres are cleaned of retained solids from time to time by back-washing the fibres by introducing a gas into the fibre lumens as the back-wash medium characterised in that the filter is a cartridge filter comprising a hollow body containing a plurality of elastic polymeric porous hollow fibres therein, the space surrounding said fibres forming the feed side of the filter, and that the fibres are cleaned by a procedure comprising introducing into the fibre lumens a pulse of a pressurised gas at a pressure sufficient to cause swelling of the pores in the fibre walls, to overcome the effect of the surface tension of the continuous phase of the feedstock within the pores of the fibre walls, and to cause explosive decompression through the walls of the fibres, the duration of said pulse of pressurised gas ranging from about 1 to 5 seconds and being sufficient to introduce through the fibre lumens a volume of

said pressurised gas such that its expanded volume exceeds the volume of the feed side of the filter so as to dislodge from the fibres into the feed side of the filter a substantial portion of the retained solids.

The penetration of gas into the pores of a membrane is resisted by the surface tension forces of the contained wall-wetting liquid according to well known theory. Indeed, surface tension is conveniently measured by the breakthrough pressure needed to force a bubble out of a submerged orifice. For common systems (such as oil in hydrophobic pores or water in hydrophilic pores) the breakthrough pressure required ranges from ten kilopascals to a thousand kilopascals. The breakthrough pressures are much higher than the usual operating pressures of the filter.

Prior art hollow-fibre type ultrafilters are usually fed from the inside of the fibres for many well known reasons. However, according to the present invention, feedstock is applied to the outside of the fibres and gas is introduced into the lumen of the fibre as the back-wash medium. In some cases, the lumen pressure swells a suitably designed fibre so that the pores are enlarged whereby the particles are freed and swept away in the expansion of the back-wash gas.

The products of our co-pending International Patent Application PCT/AU84/00179 "Treatment of Porous Membranes" are ideal for gas back-wash since they are highly elastic hydrophobic, relatively coarser porous membranes which have a tenacious hydrophilic coating and interstitial hydrophilic packing. The packing prevents pore collapse when fed under pressure from outside the porous tube. The packing is of different resilience and allows controlled expansion of the (formerly hydrophobic) pores to which it adheres. It is thus possible to design the composite fibre so that the gas release characteristics are ideal for cleaning off different types of blockage in differing configurations of fibre bundles without pressures greater than those needed to sweep away the deposits rapidly.

In some cases, especially where very fine-pored interstitial material is deposited in relatively coarse-pored base fibre, it is advantageous to back-wash first with a small amount of permeate already in the membrane lumen and follow with the high pressure gas back-wash. In this way, the small amount of permeate adequately washes out fine blocking material from within the interstices, and the overall cleaning is completed by the higher pressure gas swelling the base pores and erupting around elastic openings. The pores must close again rapidly to reseal the holes and the base material must not crack by work hardening and must remain within its modified elastic limit.

Polypropylene base is very resistant to flex cracking but is hydrophobic and rather too easy to crush. Its properties may be improved by elastic modification which can be accomplished by the method of our above-mentioned co-pending International patent application. The two inventions together synergistically improve the performance of microfilters and ultrafilters.

The use of gas as a back-wash medium enables the removal of fouling species by explosive decompression of the gas through the membrane structure for the minor part and at the outer membrane surface for the major part. Thus, the gaseous back-wash step is carried out at a pressure which is sufficient to overcome the effect of the surface tension of the continuous phase of the feedstock within the pores of the membrane.

DESCRIPTION OF PREFERRED EMBODIMENTS

In order that the invention may be more readily understood and put into practical effect, reference will now be made to the accompanying drawings in which:

- Fig. 1 shows the flux profile for an illustrative example of a gaseous back-wash system incorporating a partial permeate back-wash, and,
Fig. 2 is a schematic diagram of a gaseous back-wash cleaning system according to one embodiment of the invention.

In Fig. 1, OA represents initial permeate flux, OC the filtering time and GH the recovered permeate flux. The length CF represents the time of permeate back-wash and FG the time of gas back-wash. For a given set of operating conditions, the area ABCO depends on the rate of flux decline and length of time between successive back-wash operations. The area CDEF represents the volume of permeate back-wash.

In order to obtain optimal throughput, it is necessary to simultaneously:-

- i) maximise area ABCO,
- ii) minimise area CDEF,
- iii) optimise permeate back-wash time CF,
- iv) optimise gas back-wash time FG,
- v) maximise recovered flux GH, and,
- vi) optimise permeate back-wash flux CD.

The gaseous back-wash can be implemented in a number of ways, and one such system is shown in

Fig. 2. The filter 10 has a draw-off line 11 through which permeate normally flows to valve 12. Gas back-wash is introduced through line 13 which includes a gas pressure control valve 14, a gas flow valve 15 and a gas on/off valve 16. The filter 10 is connected to tank 17 through lines 18 and 19. The inclusion of valve 15, which controls gas flow, gives the line BD in Fig. 1 a sharp negative slope. The slower the gas flow, the shallower the (negative) slope of that line. If desired, the feed pressure may be dropped to zero before back-wash, in which case the line BD will bend at C, and BC will be vertical. This latter procedure is desirable where the gas breakthrough pressures are high, so that a lesser total pressure for the gas may be used since the liquid feed pressure does not have to be overcome.

The gas back-wash time should be sufficient to remove the fouling material from the membrane and from the body of the filter before re-application of normal process conditions. In other words, the volume of expanded gas should exceed the volume of the feed side of the hollow fibre filter. Preferably the gaseous back-wash time should exceed the residence time for feed flowing through the filter.

Gaseous back-wash can be initiated automatically by using a timer, or a flowswitch on the permeate line.

The following examples illustrate the application of the invention and the methods used to give effect to the invention of gaseous back-wash cleaning of ultrafilters.

Example 1

An ultrafilter of 0.16m² area was made according to Example 1 of our co-pending International patent application by depositing a "cross-linked polyamide" within the pores and as a network over the surface of a polypropylene ultrafilter. Within the context of this specification a "cross-linked polyamide" is one in which at least one of the group consisting of acid halides and primary and secondary amines is aromatic or substituted aromatic and the acid halide is normally used in excess to give chemical resistance and the average functionality is above two so that there is considerable cross-linking.

In Example 1 of our International patent application PCT/AU84/00179, terephthaloylchloride was used as the acid chloride and bis (3-aminopropyl) amine was used because of its solubility in hexane to provide a deposition formulation. The formulation was applied to the membrane and polyamide deposition was complete within an hour.

In order to ensure that the material deposited into the pores of the polypropylene a fine dilute emulsion was formed of size about 1 micron and of such interfacial tension with the continuous phase as to cause exclusion from the smaller pores but to allow entry into the coarser pores. The emulsion was formed as a hydrophobic mixture of:

Bis (3-aminopropyl) amine	3.93 grams
P-tertiaryoctylphenoxy-polyethyleneglycolether	0.1 grams
Petroleum spirit (b.p. 60-80°C)	950 millilitres
Absolute ethanol	50 millilitres

Water was added drop-by-drop until a distinct opalescent turbidity indicated that droplets above the wave length of visible light were present. These would, of course, be above 1 micron in size. Care was taken to apply the 1% weight per volume terephthaloylchloride solution in petroleum spirit as soon as the amine solution had evaporated to the desired film with droplets in the larger pores. The treated membrane was allowed to stand for 24 hours before fixing with the acid chloride to permit diffusion into the smaller pores as is required for thermodynamic stability.

The treated membrane was washed in a 20% weight per volume aqueous hydrochloric acid to dissolve any uncross-linked material and to hydrolyse the excess terminal acid chloride to carboxylic acid groups. A thorough water wash and drying at 60°C completed the treatment.

The filter was tested for permeability at 75kPa with the following results:

Tap water flux was 372 l/m²hr.

Wheat starch factory waste flux

EP 0 160 014 B1

initial	220 1/m ² hr.
after 30 min	162 1/m ² hr.
after 45 min	124 1/m ² hr.
after 16 hr	36 1/m ² hr.

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The seriously blocked ultrafilter was then back-washed with permeate at a pressure rising over 30 seconds to 300kPa and retested on the starch waste at 75 kPa to give a flux of 151 1/m²hr. A test showed unchanged complete rejection of 0.1% BP FEDARO M soluble cutting oil. The (slight) stretch due to the 200kPa lumen pressure was elastically recovered.

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Although this experiment did show that high pressure permeate back-wash was enhanced by the stretching of the fibres and that elastic recovery was possible, the loss of permeate was a detracting feature.

15 Example 2

In another run on starch waste at 100kPa, the above cartridge filter gave permeation rates after 24 hours of only 10 1/m²hr. Back-washing through the lumen with permeate at 150kPa and 200kPa gave no increase in permeation rates. However at 400kPa some slight swelling of the pores released particles which resulted in an initial permeation rate of 34 1/m²hr on re-testing. While the cleaning was still very incomplete there was evidence for a steeply increasing benefit as internal pressures rose to 400kPa. The reason for this was believed to be the stretching of the fibres.

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Example 3

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A larger composite cartridge (0.5m²) having hollow fibres treated as set forth in Example 1 was fed with stiff starch waste and showed that permeate back-wash did not generate enough flow to clear the accumulation from the cartridge even at 700kPa. At this latter pressure, much permeate was sacrificed in the 30 second flush back with liquid. On switching to air back-wash, no air appeared in five second trial pressures until 500kPa, when a sudden cloud of fine bubbles rapidly turned to turbulent decompression. The rapidly expanding gas increased five fold in volume and swept out the shell side of the tubes cleanly. When the shell side was kept running at 200kPa, there was a need, as expected, to raise the pressure to 700kPa to achieve the same effect. The use of air back-wash possessed the further advantage of minimising permeate loss.

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Example 4

A composite cartridge of polypropylene made hydrophilic with cross-linked polyamide gave 75% rejection of gelatin. It was used on a rapid fouling industrial waste egg mucin. Initial rates at 100kPa were 20 1/m²hr and these fell off to 12 1/m²hr in 20 minutes. A back-blow with air at 500kPa for five seconds returned rates to only 15 1/m²hr. It was noted that stringy mucin was removed efficiently. It was found that a steadily rising back-wash for five seconds with a small quantity of permeate left in the line evidently cleared the microporous filling and that the following air pulse at 500kPa peak blasted off the stringy mucin.

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In this case the small volume of permeate in the permeate line (the minimum back-wash) steadily pressurised above the feed by 500kPa, followed by three seconds of explosive gas expansion continually kept the rate at the initial 20 1/m²hr, even when the feed was concentrated threefold.

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Example 5

A 50 L sample of brine of density 1.36 was obtained from a solar pond which had concentrated seawater over a period of three years to a saturated condition. The brine was contaminated by algae and other organic materials which were required to be removed for crystallisation. The sample was pumped into a cross-flow hollow polypropylene fibre filtration cartridge. The inlet pressure was 270 kPa. The concentrate backpressure was 200 kPa and the filtrate backpressure was 5 kPa. The initial flux was 106 L/hour from the cartridge. After 13 minutes this rate had fallen to 64 L/hour and continued to decline to 50 L/hour after a further 58 minutes. The unit was then back-washed with air at 500 kPa and the flux immediately returned to 106 L/hour. This cycle was repeated.

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Example 6

A 50 L sample of hydrolized wheat starch was filtered through a 50 micron screen and the fatty acids decanted. The resulting liquor was highly turbid with a very high suspended solids and dissolved solids loading. This material was pumped into a hollow polypropylene fibre cartridge at 200 kPa with a backpressure of 160 kPa and a filtrate backpressure of 5 kPa. The initial flux of 58 L/hour declined after 24 minutes to 31 L/hour. The cartridge was then back-washed with 500 kPa air and the flux immediately returned to 58 L/hour. Over a further period of 15 minutes the flux again declined to 31 L/hour. The cartridge was again back-washed and the cycle repeated. At all times the filtrate was a clear pale brown solution.

Example 7

The 30 L sample of black water soluble ink waste from a packaging plant was pumped into a hollow polypropylene fibre cartridge at 200 kPa with a backpressure of 140 kPa and a filtrate backpressure of 5 kPa. The initial flux on commencement was 82 L/hour from the cartridge. After a period of 25 minutes this had declined to 60 L/hour. The cartridge was then back-washed with 500 kPa air and the flux returned to 82. The cycle was repeated. The filtrate at all times remained a clear pale orange colour.

Example 8

A 50 L sample of polyvinyl acetate manufacturing waste was obtained. This waste included PVA polymer as well as other waste stream constituents. It had been treated by the addition of ferric chloride and the addition of caustic to adjust the pH to 10. The floc material was then pumped into a hollow polypropylene fibre filtration cartridge at 185 kPa with a backpressure of 145 kPa. The initial throughput rate was 53 L/hour. After 7 minutes it had declined to 43 and after 20 minutes it had declined to 36 L/hour. The unit was then back-washed with 500 kPa air for eight seconds and the flux immediately returned to 52 L/hour. The rate then continued to decline until back-wash was repeated.

Example 9

A 25 L sample of unprocessed apple juice was processed through a hollow polypropylene fibre ultrafiltration unit. The inlet pressure was 70 kPa, the outlet pressure 65 kPa and the filtrate pressure 35 kPa. At the commencement of filtration the flux was 420 L/hour and after a period of two hours this declined slowly to 200 L/hour. On the application of a three second back-wash with 500 kPa air, the flux returned to 240 L/hour. After a period of another hour the flux slowly declined to 200 L/hour and a three second back-wash again returned it to 240 L/hour. At all times the filtrate quality had a clarity greater than that considered to be the best available in the industry.

Example 10

A 25 L sample of water which had been used for washing cut potatoes was collected for processing. The initial input pressure was 200 kPa, backpressure on the cartridge 150 kPa and filtrate pressure 20 kPa. When filtration commenced the flux was 132 L/hour from the hollow polypropylene fibre cartridge. After a period of 48 minutes, this flux declined to 90 L/hour. The cartridge was back-washed with 500 kPa air for five seconds and the flux returned to 120 L/hour. Over a period of another ten minutes the flux declined to 115 L/hour. The cartridge was then back-washed for five seconds and the flux was restored to 120 L/hour. The average potato starch content of the feed material was 8.6% and the average potato starch concentration in the filtrate was 0.13%.

Example 11

A sample of wheat starch hydrolysate was obtained after it had been dosed with diatomaceous earth at the rate of 63 grams per 20 L. This material was pumped into hollow polypropylene fibre filtration cartridges at an inlet pressure of 185 kPa, an outlet backpressure of 95 kPa and a filtrate backpressure of 20 kPa. The initial throughput rate of flux was 19.2 L/hour and after a period of 16 minutes this declined to 14.1 L/hour. The cartridges were then back-washed for 5 seconds with 475 kPa air and the flux was restored to 24.6 L/hour. The cartridge was then allowed to continue filtration for a further 12 minutes and the flux declined to 20.5 L/hour. Upon back-washing with air the flux was restored to 25.8 L/hour.

Various modifications may be made in details of the method of cleaning ultrafilters without departing from the scope and ambit of the invention.

Claims

- 5 1. A method of filtering a liquid suspension feedstock in a filter in which the feedstock to be filtered is applied to the outside of a plurality of porous hollow fibres having pores in the range from 5 μ m (5 micron) to 0.01 μ m (0.01 micron) and the filtrate or permeate is drawn off from the fibre lumens and in which the fibres are cleaned of retained solids from time to time by back-washing the fibres by
 10 introducing a gas into the fibre lumens as the back-wash medium characterised in that the filter is a cartridge filter comprising a hollow body containing a plurality of elastic polymeric porous hollow fibres therein, the space surrounding said fibres forming the feed side of the filter, and that the fibres are cleaned by a procedure comprising introducing into the fibre lumens a pulse of a pressurised gas at a
 15 pressure sufficient to cause swelling of the pores in the fibre walls, to overcome the effect of the surface tension of the continuous phase of the feedstock within the pores of the fibre walls, and to cause explosive decompression through the walls of the fibres, the duration of said pulse of pressurised gas ranging from about 1 to 5 seconds and being sufficient to introduce through the fibre lumens a volume of said pressurised gas such that its expanded volume exceeds the volume of the feed side of the filter so as to dislodge from the fibres into the feed side of the filter a substantial portion of the
 20 retained solids.
2. A method according to claim 1, characterised in that the porous hollow fibres have a hydrophilic coating.
- 25 3. A method according to claim 2, characterised in that the porous hollow fibres have a hydrophilic coating and a hydrophilic packing within the pores.
4. A method according to any one of claims 1 to 3, characterised in that the gaseous back-washing step is preceded by a permeate back-washing step.
- 30 5. A method according to any one of claims 1 to 4, characterised in that the pressurised gas used in the gaseous back-washing step has a pressure in the range of 10 to 800 kPa.
6. A method according to any one of claims 1 to 5, characterised in that the pressurised gas used in the
 35 gaseous back-washing step has a pressure of 500 kPa.
7. A method according to any one of claims 1 to 6, characterised in that the duration of the gaseous back-washing step exceeds the residence time for feedstock flowing through the filter.

Patentansprüche

1. Verfahren zum Filtern einer flüssigen Suspensionsbeschickung in einem Filter, bei dem die zu
 45 filtrierende Beschickung auf die Außenseite einer Vielzahl von porösen hohlen Fasern mit Poren im Bereich von 5 μ m (5 Mikron) bis 0,01 μ m (0,01 Mikron) aufgebracht wird und das Filtrat oder Permeat von den Faserlumina abgezogen wird und bei dem die Fasern von Zeit zu Zeit von zurückgehaltenen Feststoffen durch Rückwaschen der Fasern durch Einführen eines Gases in die Faserlumina als Rückwaschmedium gereinigt werden, dadurch **gekennzeichnet**, daß der Filter ein Patronenfilter ist, der einen Hohlkörper, darin enthaltend eine Vielzahl von elastischen, polymeren, porösen hohlen
 50 Fasern, umfaßt, wobei der die genannten Fasern umgebende Raum die Beschickungsseite des Filters bildet, und daß die Fasern durch eine Verfahrensweise gereinigt werden, bei der in die Faserlumina ein Impuls bzw. Stoß eines unter Druck gesetzten Gases mit einem ausreichenden Druck, daß ein Quellen der Poren in den Faserwänden bewirkt wird, eingeführt wird, um den Effekt der Oberflächenspannung der kontinuierlichen Phase der Beschickung innerhalb der Poren der Faserwände zu überwinden und um eine explosive Dekomprimierung durch die Wände der Fasern hindurch zu bewirken, wobei die
 55 Dauer des genannten Impulses bzw. Stoßes des unter Druck gesetzten Gases im Bereich von etwa 1 bis 5 Sekunden liegt und ausreichend ist, durch die Faserlumina ein derartiges Volumen des genannten unter Druck gesetzten Gases einzuführen, daß sein expandiertes Volumen das Volumen der Beschickungsseite des Filters übersteigt, so daß ein wesentlicher Teil der zurückgehaltenen Feststoffe von den

Fasern in die Beschickungsseite des Filters entfernt wird.

2. Verfahren nach Anspruch 1, dadurch **gekennzeichnet**, daß die porösen hohlen Fasern einen hydrophilen Überzug haben.
3. Verfahren nach Anspruch 2, dadurch **gekennzeichnet**, daß die porösen hohlen Fasern einen hydrophilen Überzug und eine hydrophile Packung innerhalb der Poren haben.
4. Verfahren nach einem der Ansprüche 1 bis 3, dadurch **gekennzeichnet**, daß der Gasrückwaschstufe eine Permeationsrückwaschstufe vorangeht.
5. Verfahren nach einem der Ansprüche 1 bis 4, dadurch **gekennzeichnet**, daß das in der Gasrückwaschstufe verwendete unter Druck gesetzte Gas einen Druck im Bereich von 10 bis 800 kPa hat.
6. Verfahren nach einem der Ansprüche 1 bis 5, dadurch **gekennzeichnet**, daß das in der Gasrückwaschstufe verwendete unter Druck gesetzte Gas einen Druck von 500 kPa hat.
7. Verfahren nach einem der Ansprüche 1 bis 6, dadurch **gekennzeichnet**, daß die Dauer der Gasrückwaschstufe die Verweilzeit der durch das Filter strömenden Beschickung übersteigt.

Revendications

1. Procédé de filtration d'une charge sous forme de suspension liquide dans un filtre dans lequel la charge à filtrer est appliquée à l'extérieur d'une pluralité de fibres creuses poreuses ayant des pores compris dans la plage de 5,µm (5 microns) à 0,01µm (0,01 micron) et le filtrat ou perméat est soutiré hors des lumières des fibres et dans lequel les fibres sont débarrassées de temps en temps des solides retenus par lavage des fibres à contre-courant, par introduction dans les lumières des fibres d'un gaz comme milieu de lavage à contre-courant, caractérisé en ce que le filtre est une cartouche filtrante comprenant un corps creux contenant une pluralité de fibres creuses poreuses polymères élastiques, l'espace entourant lesdites fibres formant le côté alimentation du filtre, et en ce que les fibres sont nettoyées par une technique comprenant l'introduction dans les lumières des fibres d'une pulsion d'un gaz sous pression à une pression suffisante pour provoquer le gonflement des pores dans les parois des fibres, pour surmonter l'effet de la tension superficielle de la phase continue de la charge à l'intérieur des pores des parois fibreuses et pour provoquer une décompression explosive à travers les parois des fibres, la durée de ladite pulsion de gaz sous pression étant comprise entre environ 1 et 5 s et étant suffisante pour introduire dans les lumières des fibres un volume dudit gaz sous pression tel que son volume expansé soit supérieur au volume du côté alimentation du filtre, de façon à déloger une proportion sensible des solides retenus dans les fibres dans le côté alimentation du filtre.
2. Procédé selon la revendication 1, caractérisé en ce que les fibres creuses poreuses ont un revêtement hydrophile.
3. Procédé selon la revendication 2, caractérisé en ce que les fibres creuses poreuses ont un revêtement hydrophile et une étanchéification hydrophile à l'intérieur des pores.
4. Procédé selon l'une quelconque des revendications 1 à 3, caractérisé en ce que l'étape de lavage gazeux à contre-courant est précédée par une étape de lavage à contre-courant par le perméat.
5. Procédé selon l'une quelconque des revendications 1 à 4, caractérisé en ce que le gaz sous pression utilisé au cours de l'étape de lavage gazeux à contre-courant présente une pression comprise dans la plage de 10 à 800 kPa.
6. Procédé selon l'une quelconque des revendications 1 à 5, caractérisé en ce que le gaz sous pression utilisé au cours de l'étape de lavage gazeux à contre-courant présente une pression de 500 kPa.
7. Procédé selon l'une quelconque des revendications 1 à 6, caractérisé en ce que la durée de l'étape de lavage gazeux à contre-courant est supérieure au temps de séjour nécessaire pour que la charge

EP 0 160 014 B1

traverse le filtre.

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